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1 Numerical and Experimental Analysis of Shallow Turbulent Flow over
2 Complex Roughness Beds

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26

27 **ABSTRACT**

28 A set of shallow-water equations (SWEs) based on a $\hat{k} - \hat{\varepsilon}$ Reynold stress model is established
29 to simulate the turbulent flows over a complex roughness bed. The fundamental equations are
30 discretized by the second-order finite-difference method (FDM), in which spatial and temporal
31 discretization are conducted by staggered-grid and leap-frog schemes, respectively. The
32 turbulent model in this study stems from the standard $\hat{k} - \hat{\varepsilon}$ model, but is enhanced by replacing
33 the conventional vertical production with a more rigorous and precise generation derived from
34 the energy spectrum and turbulence scales. To verify its effectiveness, the model is applied to

35 compute the turbulence in complex flow surroundings (including a rough bed) in an abrupt
36 bend and in a natural waterway. The comparison of the model results against experimental data
37 and other numerical results shows the robustness and accuracy of the present model in
38 describing hydrodynamic characteristics, especially turbulence features on the complex
39 roughness bottom.

40 **Keywords:** Energy spectrum, Roughness bed, SWE model, Shallow flows, Turbulent flows

41

42 **1 Introduction**

43 Large and small turbulent swirling flows are often clearly observable when dealing with
44 hydraulic structures in rivers and coastal areas and they are a key factor that influence the
45 frequency and magnitude of natural processes such as the sediment transport, mixing of
46 pollutants and/or riverbed deformation. Therefore, to better manage the rivers and design
47 reliable hydraulic structures, it is fundamental to understand these features and facilitate their
48 predictions. However, certain external factors (e.g. various and inconsistent boundary
49 conditions) make the characterizations of turbulent flows very challenging. To the author's
50 knowledge, there is not yet a fully accurate, time-convenient, or general numerical model to
51 completely replicate the turbulent flows and their impacts over a natural roughness bed. Despite
52 that, effective simulations of the turbulent flow for some specific scenarios have been made due
53 to the rapid progress on the numerical modeling techniques and the computing powers.

54

55 The nature of turbulence is fundamentally three-dimensional (3D). Historically, 3D approaches
56 on the turbulence modeling mainly included the Direct Numerical Simulation (DNS), Large-
57 Eddy Simulation (LES), and Reynolds-Averaged Navier-Stokes (RANS) modeling [1-4].
58 Along the rivers and coastal regions, the flow domain is quite complex and spacious, and hence
59 to characterize the flow structures it would be excessively time-consuming to apply any of these
60 three approaches, which would require a large number of grid nodes in order to provide the
61 accurate results [5]. The two-dimensional (2D) Shallow Water Equations (SWE) coupled with
62 the benchmark turbulence closure model is much faster and enables the interpretation of
63 turbulent characteristics using a smaller vertical length scale (z) as compared with the two
64 horizontal ones (x and y) in those regions [6-9]. Furthermore, to obtain more accurate and
65 repeatable results, it is also critical to select the appropriate coefficients in these turbulence
66 closure equations.

67

68 2D shallow-turbulence flow models have been extensively developed over the last decades.
69 Most of the available ones are based on the Boussinesq approximations. For example, the depth-
70 averaged eddy viscosity model suggests that eddy viscosity is the simple product of the bed
71 shear velocity and water depth [10] and the depth-averaged mixing length model accounts for
72 the influence of vertical turbulence [11]. Rastogi and Rodi [12] established the 2D standard
73 depth-averaged $\hat{k} - \hat{\varepsilon}$ turbulence model based on the 3D version described by Launder and
74 Spalding [13]. To widen the range of practical applications, some coefficients in the model
75 developed by Rastogi and Rodi were modified and new $\hat{k} - \hat{\varepsilon}$ models were introduced, as
76 presented in the other studies [14-18]. The standard $\hat{k} - \hat{\varepsilon}$ model has been demonstrated to
77 provide satisfactory results after numerous comparisons with the measured data [11,14] and it
78 is also relatively simple to use and very fast. Despite this, more progresses have been made in
79 this field and recently, Cea *et al.* [11] established a depth-averaged algebraic stress turbulence
80 model (DASM) to solve a single transport equation for each Reynolds stress without requiring
81 an isotropic assumption.

82

83 For the shallow turbulent flows on a roughness bed, the vertical velocity gradient distribution
84 is the main source of turbulence. The accuracy of its depth-averaged process directly determines
85 the numerical performance of the aforementioned $\hat{k} - \hat{\varepsilon}$ models. To date there is still area for
86 improvement due to the fact that preliminary results of the standard $\hat{k} - \hat{\varepsilon}$ model only partially
87 agree with the experimental data [12]. According to Rastogi and Rodi [12], this may be related
88 to the bottom shear stress, via the friction velocity, under the assumption of similarity in the
89 vertical velocity profiles. The depth-averaging process is a consideration only of the
90 macroscopic effects of the bottom roughness on the turbulent generations. In the classic
91 “cascade” theory of energy introduced by Richardson [19], the turbulent motion is a process of
92 energy transfer among various scales including not only the macroscale, but also various
93 microscales [2, 20, 21]. The contribution of these features should be rigorously and precisely
94 replicated within turbulent closure models.

95

96 The turbulent structure of various scales based on the framework of energy cascade can be
97 divided into the energy-containing, inertial, and dissipative regions, respectively. The kinetic
98 energy, produced in the energy-containing region, is considered to be transferred by inertial
99 forces to smaller scales until the energy is typically dissipated by the molecular viscosity [2].
100 The energy spectrum in the inertial region has a universal statistical form, i.e. the Kolmogorov
101 -5/3 spectrum [22], and can be applied to larger or smaller wave numbers as the Reynolds
102 number increases [8]. Nezu and Nakagawa [20] analogized the energy transfer processes to

103 open-channel flows and divided the whole water depth into the three regions: wall,
104 intermediate, and free-surface zones. A universal log-law in the intermediate region was
105 verified by the extensive experimental and numerical results and they confirmed this can be
106 applied to a wider range of bed roughness and Reynolds numbers.

107

108 Taking into considerations all of these previous works and the new insights that have been
109 provided, this study aims to improve the performance of the standard $\hat{k}-\hat{\varepsilon}$ model to
110 characterise the generation of turbulent conditions at various scales over complex roughness
111 beds. The numerical SWE model utilised in this work includes a second-order leap-frog finite-
112 difference method (FDM) and it is built into a staggered-grid system. This model was initially
113 developed by Cho [23] to calculate the evolution of the long waves and was further extended
114 by Lin [24] to simulate the turbulent structures within an experimental zone. Lately this
115 turbulence model has been widely used to compute the complex flows induced by irregular
116 geometries and the results obtained have proven that it is a robust numerical technique [25-27].
117 In the present study, we emphasized the improvement of the model for application to the
118 complex roughness beds.

119

120 The paper is organized as follows: *Section 2* presents the description of the mathematical and
121 numerical shallow turbulence model considered for this study, clarifying various assumptions
122 and hypothesis: the governing equations are presented in *Section 2.1*, then the vertical turbulent
123 production is formulated in *Section 2.2* by incorporating the energy transfer information
124 between various scales into P_{kV} and $P_{\varepsilon V}$ based on the two universal semi-theoretical formulas
125 of Kolmogorov -5/3 scaling law and log-law. *Section 3* includes the validation of the numerical
126 model against the experimental data collected on a flume, where varying roughness on the bed
127 was tested with a complex sharp bend. Finally, to further demonstrate the potentials of the
128 model, its performance was more vigorously examined in the transport of moraine along the
129 Yangtze River under dry seasons, and the results are explained in *Section 4*. *Section 5* provides
130 a brief summary and concluding remarks of the whole study.

131 **2 Numerical Model**

132 **2.1 Governing equations**

133 This section presents the governing equations and the boundary conditions utilised in this study.

134 *2.1.1 Shallow-water equations*

135 The time-dependent SWEs are the fundamental hydrodynamic equations described in this

136 section. By integrating the Reynolds Averaged Navier-Stokes (RANS) equations along the
 137 entire water depth and assuming the vertical flow to be nearly-uniform and pressure
 138 distributions to be hydrostatic, the SWEs can be given as follows [25-27]:

$$139 \quad \frac{\partial H}{\partial t} + \frac{\partial P}{\partial x} + \frac{\partial Q}{\partial y} = 0 \quad (1a)$$

$$140 \quad \frac{\partial P}{\partial t} + \frac{\partial}{\partial x} \left(\frac{P^2}{H} \right) + \frac{\partial}{\partial y} \left(\frac{PQ}{H} \right) + gH \frac{\partial \eta}{\partial x} = \frac{1}{\rho} \frac{\partial (HT_{xx})}{\partial x} + \frac{1}{\rho} \frac{\partial (HT_{yx})}{\partial y} - \frac{f}{8H^2} \sqrt{P^2 + Q^2} P - \frac{2}{3} \frac{\partial (H\hat{k})}{\partial x} \quad (1b)$$

$$141 \quad \frac{\partial Q}{\partial t} + \frac{\partial}{\partial x} \left(\frac{PQ}{H} \right) + \frac{\partial}{\partial y} \left(\frac{Q^2}{H} \right) + gH \frac{\partial \eta}{\partial y} = \frac{1}{\rho} \frac{\partial (HT_{xy})}{\partial x} + \frac{1}{\rho} \frac{\partial (HT_{yy})}{\partial y} - \frac{f}{8H^2} \sqrt{P^2 + Q^2} Q - \frac{2}{3} \frac{\partial (H\hat{k})}{\partial y} \quad (1c)$$

142 where $H(=\eta - z_b)$ is the water depth, in which η and z_b are the free surface and bed elevation,
 143 respectively (Fig. 1); $P(=HU)$ and $Q(=HV)$ are components of unit volume flux, in which

144 $U \left(= \frac{1}{H} \int_{z_b}^{\eta} \langle u \rangle dz \right)$ and $V \left(= \frac{1}{H} \int_{z_b}^{\eta} \langle v \rangle dz \right)$ are the depth-averaged velocities in x and y directions,

145 respectively; g is gravitational acceleration; ρ is fluid density; $\hat{k} \left(= \frac{1}{H} \int_{z_b}^{\eta} k dz \right)$ is the depth-

146 averaged turbulent energy; T_{xx} , T_{yy} , T_{yx} , and T_{xy} are the depth-averaged effective stresses
 147 expressed as follows [25-26]:

$$148 \quad T_{xx} = 2\rho \frac{\nu + \hat{\nu}_t}{H} \frac{\partial P}{\partial x} \quad (2a)$$

$$149 \quad T_{yy} = 2\rho \frac{\nu + \hat{\nu}_t}{H} \frac{\partial Q}{\partial y} \quad (2b)$$

$$150 \quad T_{yx} = T_{xy} = \rho \frac{\nu + \hat{\nu}_t}{H} \left(\frac{\partial P}{\partial y} + \frac{\partial Q}{\partial x} \right) \quad (2c)$$

151 where ν and $\hat{\nu}_t$ are the kinematic viscosity and the depth-averaged turbulent viscosity,
 152 respectively, as defined in Eq. (4).

153

154 f in Eq. (1) is the bed friction factor defined according to parameters for the smooth and rough
 155 beds previously obtained [26, 28], such as Chézy-Manning's and Altsul's formula:

$$156 \quad f = \frac{8gm^2}{H^{1/3}} \quad (3a)$$

$$157 \quad f = 0.1 \left(1.46 \frac{k_s}{R} + \frac{100}{Re} \right)^{1/4} \quad (3)$$

158 b)

159 where m is Manning's roughness coefficient; k_s is bed roughness height, which in this study
 160 it is considered to be the median diameter of the bed material; R is the hydraulic radius (the
 161 water depth, in this study); and Re is the Reynolds number.

162 2.1.2 Depth-averaged $\hat{k} - \hat{\varepsilon}$ closure equations

163 The depth-averaged velocity field in Eq. (1) can be solved when \hat{v}_t is determined. The
 164 specification of \hat{v}_t is assumed to be mathematically analogous to the turbulent viscosity ν_t in
 165 the standard $k - \varepsilon$ model [25], and can be expressed as follows:

$$166 \quad \hat{v}_t = C_\mu \frac{\hat{k}^2}{\hat{\varepsilon}} \quad (4)$$

167 The transport equations \hat{k} and $\hat{\varepsilon}$ can be then introduced, respectively, as follows:

$$168 \quad \frac{\partial(H\hat{k})}{\partial t} + \frac{\partial(P\hat{k})}{\partial x} + \frac{\partial(Q\hat{k})}{\partial y} = H\hat{v}_t \left[2 \left(\frac{\partial U}{\partial x} \right)^2 + 2 \left(\frac{\partial V}{\partial y} \right)^2 + \left(\frac{\partial U}{\partial y} + \frac{\partial V}{\partial x} \right)^2 \right] + P_{kV} + \quad (5a)$$

$$\frac{\partial}{\partial x} \left[\left(\nu + \frac{\hat{v}_t}{\sigma_k} \right) \frac{\partial(H\hat{k})}{\partial x} \right] + \frac{\partial}{\partial y} \left[\left(\nu + \frac{\hat{v}_t}{\sigma_k} \right) \frac{\partial(H\hat{k})}{\partial y} \right] - H\hat{\varepsilon}$$

$$169 \quad \frac{\partial(H\hat{\varepsilon})}{\partial t} + \frac{\partial(P\hat{\varepsilon})}{\partial x} + \frac{\partial(Q\hat{\varepsilon})}{\partial y} = C_{\varepsilon 1} \frac{\hat{\varepsilon}}{\hat{k}} H\hat{v}_t \left[2 \left(\frac{\partial U}{\partial x} \right)^2 + 2 \left(\frac{\partial V}{\partial y} \right)^2 + \left(\frac{\partial U}{\partial y} + \frac{\partial V}{\partial x} \right)^2 \right] + \quad (5b)$$

$$P_{\varepsilon V} + \frac{\partial}{\partial x} \left[\left(\nu + \frac{\hat{v}_t}{\sigma_\varepsilon} \right) \frac{\partial(H\hat{\varepsilon})}{\partial x} \right] + \frac{\partial}{\partial y} \left[\left(\nu + \frac{\hat{v}_t}{\sigma_\varepsilon} \right) \frac{\partial(H\hat{\varepsilon})}{\partial y} \right] - C_{\varepsilon 2} H \frac{\hat{\varepsilon}^2}{\hat{k}}$$

170 where C_μ , σ_k , σ_ε , $C_{1\varepsilon}$ and $C_{2\varepsilon}$ are the empirical constants and their values, as recommended by
 171 Launder and Spalding [13], are

$$172 \quad C_\mu = 0.09, \sigma_k = 1.0, \sigma_\varepsilon = 1.3, C_{1\varepsilon} = 1.44, C_{2\varepsilon} = 1.92 \quad (6)$$

173 and, as suggested in [8], [12] and [13],

$$174 \quad P_{kV} = \frac{n^2 g}{H^3} (U^2 + V^2)^{3/2} \quad (7a)$$

$$175 \quad P_{\varepsilon V} = \frac{C_2 C_\mu n^2 g^5}{H^{17/12}} (U^2 + V^2)^2 \quad (7b)$$

177 2.2 Vertical turbulent production P_{kV} and $P_{\varepsilon V}$

178 P_{kV} and $P_{\varepsilon V}$ in Eq. (5) are the components generated by turbulence and can be defined as the
 179 tensor product of the horizontal Reynolds stress and vertical velocity gradient, respectively. In
 180 the context of homogeneous, open-channel turbulence, they represent all the turbulent energy
 181 produced. The corresponding expressions to calculate their magnitude were deduced by Rastogi
 182 and Rodi [12], although their derivations seemed to have overgeneralized the generation of
 183 vertical turbulent features.

184

185 According to the theory of cascade energy, which has been proven and validated against
 186 extensive experimental studies, the turbulent motion is a one-way energy transfer process from
 187 large scale eddies to smaller ones [2]. The theory can also be applied to the transfer of energy
 188 from the bottom of the river to the free surface [20]. To rigorously and precisely quantify the
 189 energy transfer across various scales, this study presents an additional model that estimates the
 190 generation of vertical turbulent features in a different manner, considering the interaction
 191 between points at different levels and the total energy spectrum. Bottom roughness elements
 192 markedly affect the amount of turbulence. Turbulence tends to be isotropy as the bed roughness
 193 and Reynolds numbers increase [2, 20,29]. Cea *et al.* [11] found a similar degree of accuracy
 194 between the $\hat{k} - \hat{\varepsilon}$ model, which is based on the concise isotropic hypothesis, and the DASM
 195 model, which includes complex model structures considering anisotropy. Based on this
 196 assumption, below are listed the steps selected to deduce the expressions of P_{kV} and $P_{\varepsilon V}$.

197 2.2.1 Mean velocity profiles

198 For a uniform and fully-developed turbulent flow in a wide open channel, the Reynolds
 199 equation in the z -direction (as derived from the Navier-Stokes equations) is reduced to:

$$200 \quad \rho \nu \frac{d\langle u \rangle}{dz} - \rho \langle u'w' \rangle = \rho u_*^2 \left(1 - \frac{z}{H} \right) \quad (8)$$

201 where $\rho \nu d\langle u \rangle / dz$ is the viscous stress; $-\rho \langle u'w' \rangle$ is the Reynolds stress; $u_* (= \sqrt{\tau_b / \rho})$ is the
 202 friction velocity, in which τ_b is the bed shear stress at $z = 0$.

203

204 By considering the Prandtl's mixing-length hypothesis, ν can be expressed as the product of a
 205 velocity scale u^* and a length scale l_m , in which u^* is specified as $u^* = |\langle u'w' \rangle|^{1/2}$. From Eq. (8),

206 the following equation could be obtained:

$$207 \quad \frac{d\langle u \rangle^+}{dz^+} = \frac{2\tau/\tau_b}{1 + \sqrt{1 + (4\tau/\tau_b)(l_m^+)^2}} \quad (9)$$

208 where $\langle u \rangle^+ = \langle u \rangle / u_*$ and $z^+ = zu_* / \nu_k$ are the dimensionless velocity and z -coordinate
 209 normalized by the viscous length $\delta_v = \nu_k / u_*$, respectively; $l_m^+ = l_m u_* / \nu_k$ is the dimensionless
 210 mixing-length. If appropriate specification of l_m^+ over the whole depth can be obtained, Eq. (9)
 211 can be easily integrated to yield the distribution of $\langle u \rangle$.

212

213 In various regions from $z=0$ to $z=\eta$, the effect of $\rho\nu d\langle u \rangle/dz$ and $-\rho\langle u'w' \rangle$ on the
 214 velocity distribution is different. According to their contribution to the turbulent structure, the
 215 vertical turbulence fields of $\langle u \rangle$ are divided into two regions: the inner region and the outer
 216 region [20]. It is assumed that the viscous effect dominates the inner region (in general,
 217 $z/H < (0.15-0.2)$), so the length scale can be denoted by δ_v . The component τ/τ_w tends
 218 towards unity and l_m^+ can be specified as $l_m^+ = \kappa z^+$ in this region, so the solution to Eq. (9) (the
 219 “log-law”), can be obtained as follows:

$$220 \quad \langle u \rangle^+ = \frac{1}{\kappa} \ln z^+ + A \quad (10)$$

221 where $\kappa = 0.40-0.43$ and $B = 5.2$ are the empirical constants [2, 30].

222

223 It is assumed that the viscous contribution in the outer region (generally, $z/H \geq (0.15-0.2)$) to
 224 the turbulent structure is negligible, and that l_m^+ no longer depends on δ_v . It is challenging to
 225 solve Eq. (9) because there is no universal representation of l_m^+ . The wake law provided by
 226 Coles [31], is typically used to extend the log-law to the outer region. The profile of $\langle u \rangle$ in this
 227 region can be approximated as follows:

$$228 \quad \langle u \rangle^+ = \frac{1}{\kappa} \ln z^+ + A + \frac{2\Pi}{\kappa} \sin^2\left(\frac{\pi z}{2H}\right) \quad (11)$$

229 where Π is Coles’s wake-strength parameter. Π has been investigated in various studies where
 230 its value has been suggested to be around 0.08-0.20. Π also shows no distinct value for flows
 231 with different bed roughness conditions [32]. Considering the comparisons made by Pope [2]
 232 and Nezu and Nakagawa [20], the profile of $\langle u \rangle$ can be effectively approximated by Eq. (11)
 233 over the whole depth except in a small region near the bed. In the core region of closed-bed

234 flow (e.g., $z^+ < 26$), l_m^+ is strongly affected by the Reynolds number and bed roughness, so
 235 $\langle u \rangle$ is likely to remain the complex profile. In this study, we considered the distribution of $\langle u \rangle$
 236 in this region to be determined by using Eq. (11).

237 2.2.2 Depth-averaged vertical production

238 Based on Kolmogorov's scaling theory outlined at [22], the dissipation rate ε could be related
 239 to $\|u'\|$ by using the macroscale of turbulence described in [20, 21] as follows:

$$240 \quad \varepsilon = K \frac{\|u'\|^3}{L_x} \quad (12)$$

241 where $K = [2/(\pi C')]^{3/2} (L_x k_0)^{5/2}$ is a turbulent coefficient which is greatly influenced by the
 242 Reynolds number, C' is a universal Kolmogorov constant, L_x is the longitudinal integral
 243 macroscale, k_0 is macroscale of turbulence. Nakagawa et al. [33] suggested that $\|u'\|/u_*$ can be
 244 approximated as the power function of z/H :

$$245 \quad \frac{\|u'\|}{u_*} = \left[\frac{B_N}{\kappa K} \left(1 - \frac{z}{H} \right) \right]^{1/3} \left(\frac{z}{H} \right)^{-1/6} \quad (13)$$

246 Further, under an assumption of isotropy, Nezu and Nakagawa [20] found that the correlation
 247 coefficients of turbulence intensities are nearly constant as long as z^+ is sufficiently large. This
 248 can be approximately represented by:

$$249 \quad \|w'\|/\|u'\| = C_1, \|v'\|/\|u'\| = C_2 \quad (14)$$

250 where C_1 and C_2 are empirical constants.

251

252 For stationary and homogeneous turbulence, the turbulent production $P_k (= -\langle u'w' \rangle \partial \langle u \rangle / \partial z)$ is
 253 balanced approximately by the sum of the turbulent diffusion $D_k (= (d/dz) [(v/\sigma_k) (dk/dz)])$
 254 and dissipation ε independently of the molecular diffusion. In the inertial subrange, energy
 255 transfer is the only significant process; there is no energy production or dissipation. Thus,
 256 $P_k \approx \varepsilon$. The dynamic equilibrium of turbulent energy can then be expressed as follows:

$$257 \quad v \frac{dk}{dz} = \text{const.} \quad (15)$$

258 in which $v (= C_\mu k^2 / \varepsilon)$ is the turbulent viscosity. Substituting Eq. (12) into v (where L_x is of
 259 the same order as H) and making use of Eq. (14) (where u' is of the order of u_*) yields the

260 following approximation of ν :

$$261 \quad \nu \approx \frac{1}{k} H u_*^3 \quad (16)$$

262 Substituting Eq. (16) into Eq. (15) with the integral from 0 to z yields the distribution of k :

$$263 \quad \frac{k}{u_*^2} = D \exp\left(-2C_k \frac{z}{H}\right) \quad (17)$$

264 where D and C_k are the constants. Applying Eqs. (14) and (17) provides the profiles of u' , v'
265 , and w' :

$$266 \quad \frac{\|u'\|}{u_*} = D_u \exp\left(-C_k \frac{z}{H}\right) \quad (18a)$$

$$267 \quad \frac{\|v'\|}{u_*} = D_v \exp\left(-C_k \frac{z}{H}\right) \quad (18b)$$

$$268 \quad \frac{\|w'\|}{u_*} = D_w \exp\left(-C_k \frac{z}{H}\right) \quad (18c)$$

269 where D_u, D_v, D_w , and C_k are the empirical constants; their values are 2.30, 1.27, 1.63, and
270 1.0, respectively [20].

271

272 By closely examining the turbulence intensities presented by Nezu and Nakagawa [20], we
273 found close agreement between Eq. (18) results and the experimental values throughout the
274 whole depth apart from a thin layer near the bed. Surprisingly, any deviation between them
275 gradually decreased as Re and k_s^+ ($= k_s u_* / \nu_k$) increased. To some extent, Eq. (18) is
276 successful in displaying the vertical distribution of turbulence intensity. Integrating Eq. (18)
277 with the given empirical constants allows the depth-averaged turbulent energy \hat{k} to be obtained:

$$278 \quad \hat{k} = 2.07 u_*^2 \quad (19)$$

279 The constant used in Eq. (19) has been found by combining D_u, D_v , and D_w at Eqs. (18a)–(18c),
280 suggested in Nezu and Nakagawa [20]. The formulation of k is described in Eq. (37). According
281 to the theory of cascade energy, at the end of the sequence of processes, the dissipation of
282 turbulent energy is accomplished primarily by molecular viscosity. In other words, the energy
283 of open-channel flows is predominantly dissipated in the free surface region. Observed ε
284 values in this region are less accurate due to the constraints of free-surface fluctuations. In the
285 comparison made by Nakagawa et al. [33], it is very difficult to obtain a universal formula for
286 ε . In this study, we used ν as a replacement for ε to determine P_{kV} and $P_{\varepsilon V}$.

287

288
$$v = \frac{\kappa(1-z/H)Hu_*}{(H/z) + \pi\Pi \sin(\pi z/H)} \quad (20)$$

289 Eq. (20) is found from substituting Coles' law at Eq. (11) into Eq. (8). By integrating Eq. (20)
 290 from the bed to free surface, we obtained the depth-averaged turbulent viscosity \hat{v}_t as follows:

291
$$\hat{v}_t = 0.06Hu_* \quad (21)$$

292 The constant in Eq. (21) comes from depth-averaging Eq. (20) from bed to free-surface, using
 293 described values of κ and Π in section 2.2.1. In stationary and homogeneous flows, P_{kV} and

294 $P_{\varepsilon V}$ in the $\hat{k} - \hat{\varepsilon}$ transport equations are balanced only by their dissipation terms $\hat{\varepsilon}H$ and
 295 $C_{2\varepsilon} \hat{\varepsilon}^2 H / \hat{k}$, respectively. P_{kV} and $P_{\varepsilon V}$ can be obtained by rearranging Eq. (5) and combining
 296 Eqs. (4), (19) and (21):

297
$$P_{kV} = 71.42 C_\mu u_*^3 \quad (22a)$$

298
$$P_{\varepsilon V} = 2464.16 C_\mu^2 C_{2\varepsilon} \frac{u_*^4}{H} \quad (22b)$$

299 where $u_* = \sqrt{f(U^2 + V^2)}/8$. These Eqs. (22a) and (22b) have been derived from the standard
 300 $\hat{k} - \hat{\varepsilon}$ formulations of P_{kV} and $P_{\varepsilon V}$ terms as showing at Eqs. (7a) and (7b).

301

302 2.3 Numerical implementation

303 In this study, we discretized the fundamental equations using the explicit leap-frog FDM which
 304 has second-order accuracy in both time and space [25-26]. As plotted in Fig. 2, all of the vectors
 305 (P , Q , U , and V) were evaluated at the faces of the grid; all of the scalars (H , η , z_b , \hat{k} , and $\hat{\varepsilon}$)
 306 were defined at the center of the grid. The defined location of the normal stresses (e.g.,
 307 T_{xx} and T_{yy}) is the same as the scalar; the shear stresses (e.g., T_{xy} and T_{yx}) were calculated as
 308 shown in the right-top corner of the grid.

309 2.3.1 Continuity equation

310 According to the spatial staggered grid system and the temporal leap-frog scheme, the
 311 continuity equation is explicitly discretized as follows:

312
$$H_{i,j}^{n+1/2} = H_{i,j}^{n-1/2} - \frac{\Delta t}{\Delta x_i} (P_{i+1/2,j}^n - P_{i-1/2,j}^n) - \frac{\Delta t}{\Delta y_j} (Q_{i,j+1/2}^n - Q_{i,j-1/2}^n) \quad (23)$$

313 2.3.2 Momentum equations

314 Without loss of generality, only the discretized form of x -momentum equation is presented here
 315 in detail:

$$\begin{aligned}
P_{i+1/2,j}^{n+1} &= \frac{1 - \frac{f\Delta t}{16(H_{i+1/2,j}^n)^2} \left[(P_{i+1/2,j}^n)^2 + (Q_{i+1/2,j}^n)^2 \right]^{1/2}}{1 + \frac{f\Delta t}{16(H_{i+1/2,j}^n)^2} \left[(P_{i+1/2,j}^n)^2 + (Q_{i+1/2,j}^n)^2 \right]^{1/2}} P_{i+1/2,j}^n \\
&- \frac{\Delta t}{1 + \frac{f\Delta t}{16(H_{i+1/2,j}^n)^2} \left[(P_{i+1/2,j}^n)^2 + (Q_{i+1/2,j}^n)^2 \right]^{1/2}} \left\{ \left[\frac{\partial}{\partial x} \left(\frac{P^2}{H} \right) \right]_{i+1/2,j}^n + \left[\frac{\partial}{\partial y} \left(\frac{PQ}{H} \right) \right]_{i+1/2,j}^n \right\} \quad (24) \\
&- \frac{g\Delta t}{\left\{ 1 + \frac{f\Delta t}{16(H_{i+1/2,j}^n)^2} \left[(P_{i+1/2,j}^n)^2 + (Q_{i+1/2,j}^n)^2 \right]^{1/2} \right\} \Delta x_{i+1/2}} H_{i+1/2,j}^{n+1/2} (\eta_{i+1,j}^{n+1/2} - \eta_{i,j}^{n+1/2}) \\
&+ \frac{\Delta t / \rho}{1 + \frac{f\Delta t}{16(H_{i+1/2,j}^n)^2} \left[(P_{i+1/2,j}^n)^2 + (Q_{i+1/2,j}^n)^2 \right]^{1/2}} \left[\frac{\partial(HT_{xx})}{\partial x} + \frac{\partial(HT_{yx})}{\partial y} \right]_{i+1/2,j}^n
\end{aligned}$$

317 where the convection terms are respectively discretized as follows by applying the upwind
318 scheme:

$$\left[\frac{\partial}{\partial x} \left(\frac{P^2}{H} \right) \right]_{i+1/2,j}^n = \begin{cases} \frac{\frac{(P_{i+1/2,j}^n)^2}{H_{i+1/2,j}^n} - \frac{(P_{i-1/2,j}^n)^2}{H_{i-1/2,j}^n}}{\Delta x_i} & \text{if } P_{i+1/2,j}^n > 0 \\ \frac{\frac{(P_{i+3/2,j}^n)^2}{H_{i+3/2,j}^n} - \frac{(P_{i-1/2,j}^n)^2}{H_{i-1/2,j}^n}}{\Delta x_i + \Delta x_{i+1}} & \text{if } P_{i+1/2,j}^n = 0 \\ \frac{\frac{(P_{i+3/2,j}^n)^2}{H_{i+3/2,j}^n} - \frac{(P_{i+1/2,j}^n)^2}{H_{i+1/2,j}^n}}{\Delta x_{i+1}} & \text{if } P_{i+1/2,j}^n < 0 \end{cases} \quad (25a)$$

$$\left[\frac{\partial}{\partial y} \left(\frac{PQ}{H} \right) \right]_{i+1/2,j}^n = \begin{cases} \frac{\frac{(PQ)_{i+1/2,j}^n}{H_{i+1/2,j}^n} - \frac{(PQ)_{i+1/2,j-1}^n}{H_{i+1/2,j-1}^n}}{\Delta y_{j-1/2}} & \text{if } Q_{i+1/2,j}^n > 0 \\ \frac{\frac{(PQ)_{i+1/2,j+1}^n}{H_{i+1/2,j+1}^n} - \frac{(PQ)_{i+1/2,j-1}^n}{H_{i+1/2,j-1}^n}}{\Delta y_{j-1/2} + \Delta y_{j+1/2}} & \text{if } Q_{i+1/2,j}^n = 0 \\ \frac{\frac{(PQ)_{i+1/2,j+1}^n}{H_{i+1/2,j+1}^n} - \frac{(PQ)_{i+1/2,j}^n}{H_{i+1/2,j}^n}}{\Delta y_{j+1/2}} & \text{if } Q_{i+1/2,j}^n < 0 \end{cases} \quad (25b)$$

321 2.3.3 Turbulent transport equations

322 The $\hat{\varepsilon}$ - and \hat{k} -equations are respectively discretized by applying a semi-implicit scheme:

$$323 \quad \hat{\varepsilon}_{i,j}^{n+1/2} = \frac{\frac{(H\hat{\varepsilon})_{i,j}^{n-1/2}}{\Delta t} - F\hat{\varepsilon}X - F\hat{\varepsilon}Y + VIS\hat{\varepsilon}X + VIS\hat{\varepsilon}Y + C_{1\varepsilon} \frac{\hat{\varepsilon}_{i,j}^{n-1/2}}{\hat{k}_{i,j}^{n-1/2}} (P_h)_{i,j}^{n+1/2} + (P_{\varepsilon V})_{i,j}^{n+1/2}}{\frac{H_{i,j}^{n+1/2}}{\Delta t} + C_{2\varepsilon} \frac{\hat{\varepsilon}_{i,j}^{n-1/2}}{\hat{k}_{i,j}^{n-1/2}} H_{i,j}^{n-1/2}} \quad (26a)$$

$$324 \quad \hat{k}_{i,j}^{n+1/2} = \frac{\frac{(H\hat{k})_{i,j}^{n-1/2}}{\Delta t} - F\hat{k}X - F\hat{k}Y + VIS\hat{k}X + VIS\hat{k}Y + (P_h)_{i,j}^{n+1/2} + (P_{kV})_{i,j}^{n+1/2}}{\frac{H_{i,j}^{n+1/2}}{\Delta t} + C_{\mu} \frac{\hat{\varepsilon}_{i,j}^{n-1/2}}{(\hat{\nu}_t)_{i,j}^{n-1/2}} H_{i,j}^{n-1/2}} \quad (26b)$$

325

326 Similarly, the upwind scheme can be used to discretize the convective term $F\hat{\varepsilon}X$ (the
327 differences of $F\hat{\varepsilon}Y$, $F\hat{k}X$, and $F\hat{k}Y$ are similar to $F\hat{\varepsilon}X$) as follows:

$$328 \quad [F\hat{\varepsilon}X]_{i,j}^{n-1/2} = \left[\frac{\partial(P\hat{\varepsilon})}{\partial x} \right]_{i,j}^{n-1/2} = \begin{cases} \frac{P_{i,j}^{n-1/2} \hat{\varepsilon}_{i,j}^{n-1/2} - P_{i-1,j}^{n-1/2} \hat{\varepsilon}_{i-1,j}^{n-1/2}}{\Delta x_{i-1/2}} & \text{if } P_{i,j}^{n-1/2} > 0 \\ \frac{P_{i+1,j}^{n-1/2} \hat{\varepsilon}_{i+1,j}^{n-1/2} - P_{i-1,j}^{n-1/2} \hat{\varepsilon}_{i-1,j}^{n-1/2}}{\Delta x_{i-1/2} + \Delta x_{i+1/2}} & \text{if } P_{i,j}^{n-1/2} = 0 \\ \frac{P_{i+1,j}^{n-1/2} \hat{\varepsilon}_{i+1,j}^{n-1/2} - P_{i,j}^{n-1/2} \hat{\varepsilon}_{i,j}^{n-1/2}}{\Delta x_{i+1/2}} & \text{if } P_{i,j}^{n-1/2} < 0 \end{cases} \quad (27)$$

329

330 The central difference method was applied to discretize the diffusion term $VIS\hat{\varepsilon}X$ (the
331 difference forms of $VIS\hat{\varepsilon}Y$, $VIS\hat{k}X$, and $VIS\hat{k}Y$ are analogous to $VIS\hat{\varepsilon}X$) as follows:

$$332 \quad VIS\hat{\varepsilon}X = \frac{1}{\Delta x_i} \left\{ \left[\left(v_k + \frac{\hat{\nu}_t}{\sigma_\varepsilon} \right) \frac{\partial(H\hat{\varepsilon})}{\partial x} \right]_{i+1/2,j}^{n-1/2} - \left[\left(v_k + \frac{\hat{\nu}_t}{\sigma_\varepsilon} \right) \frac{\partial(H\hat{\varepsilon})}{\partial x} \right]_{i-1/2,j}^{n-1/2} \right\} = \frac{1}{\Delta x_i} \left[\left(v_k + \frac{(\hat{\nu}_t)_{i+1/2,j}^{n-1/2}}{\sigma_\varepsilon} \right) \frac{H_{i+1,j}^{n-1/2} \hat{\varepsilon}_{i+1,j}^{n-1/2} - H_{i,j}^{n-1/2} \hat{\varepsilon}_{i,j}^{n-1/2}}{\Delta x_{i+1/2}} - \left(v_k + \frac{(\hat{\nu}_t)_{i-1/2,j}^{n-1/2}}{\sigma_\varepsilon} \right) \frac{H_{i,j}^{n-1/2} \hat{\varepsilon}_{i,j}^{n-1/2} - H_{i-1,j}^{n-1/2} \hat{\varepsilon}_{i-1,j}^{n-1/2}}{\Delta x_{i-1/2}} \right] \quad (28)$$

333 The horizontal velocity-gradient production term P_h can be discretized as:

$$334 \quad (P_h)_{i,j}^{n+1/2} = H_{i,j}^{n+1/2} (\hat{\nu}_t)_{i,j}^{n-1/2} \left[2 \left(\frac{U_{i+1/2,j}^{n+1/2} - U_{i-1/2,j}^{n+1/2}}{\Delta x_i} \right)^2 + 2 \left(\frac{V_{i,j+1/2}^{n+1/2} - V_{i,j-1/2}^{n+1/2}}{\Delta y_j} \right)^2 + \left(\frac{V_{i+1/2,j}^{n+1/2} - V_{i-1/2,j}^{n+1/2}}{\Delta x_i} + \frac{U_{i,j+1/2}^{n+1/2} - U_{i,j-1/2}^{n+1/2}}{\Delta y_j} \right)^2 \right] \quad (29)$$

335 According to the expression of Eq. (22b), the vertical velocity-gradient production term $P_{\varepsilon V}$
336 (the difference form of P_{kV} is the same as $P_{\varepsilon V}$) can be discretized as:

$$337 \quad (P_{\varepsilon V})_{i,j}^{n+1/2} = 2464.16 C_{\mu}^2 C_{2\varepsilon} \frac{\left\{ \frac{f}{8} \left[(U_{i,j}^{n+1/2})^2 + (V_{i,j}^{n+1/2})^2 \right] \right\}^2}{H_{i,j}^{n+1/2}} \quad (30)$$

338 **2.4 Boundary conditions**

339 To perform the staggered-grid difference method, ghost cells are typically imposed around the
 340 outmost computational domain. The boundary of all scalar variables, e.g., η^B , \hat{k}^B , and $\hat{\varepsilon}^B$
 341 (where the superscript B denotes the boundary) is set at the center of the ghost grid; the
 342 boundary of all vector variables, e.g., P^B and Q^B , is located at the center of the adjacent
 343 surface between the ghost cell and the outermost computational grid [27]. The boundary
 344 conditions selected for this study mainly include open boundaries and no-slip boundaries.

345

346 Open boundary conditions are applied mainly to inflow and outflow. For the tests conducted,
 347 subcritical flow is the most frequent, hence the boundary conditions assumed include a specific
 348 flow rate assigned at the upstream boundary location; in addition, uniform water depth is
 349 applied as the downstream boundary condition. The inflow boundary condition can be
 350 expressed as follows:

$$351 \quad \eta_1^B = \eta_2^B, P_{3/2}^B = P_{5/2}^B, Q_1^B = Q_2^B, \hat{k}_1^B = \hat{k}_2^B \text{ and } \hat{\varepsilon}_1^B = \hat{\varepsilon}_2^B \quad (31a)$$

352 The outflow boundary condition can be expressed follows:

$$353 \quad \eta_n^B = \eta_{n-1}^B, P_{n-1/2}^B = P_{n-3/2}^B, Q_n^B = Q_{n-1}^B, \hat{k}_n^B = \hat{k}_{n-1}^B \text{ and } \hat{\varepsilon}_n^B = \hat{\varepsilon}_{n-1}^B \quad (31b)$$

354 No-slip boundary conditions are applied on the side where there is the solid-wall. The flux on
 355 the solid boundary is zero, i.e., $P_{l+1/2}^B = Q_{l+1/2}^B = 0$, where the subscript $l+1/2$ denotes the
 356 adjacent surface between the water and solid-wall cells and l denotes the corresponding center
 357 of the wall cell. The boundary conditions for \hat{k} and $\hat{\varepsilon}$ at the location l are also necessary.

358

359 According to the boundary-layer theory, if the distance s between l and $l+1/2$ is sufficiently
 360 small, the shear stress and the turbulent production at l can be balanced approximately with
 361 the wall shear stress and the dissipation at $l+1/2$, respectively [13]. The depth-averaged
 362 statistic characteristics in the small region near the wall are assumed to be analogous to the
 363 turbulent features in the core region near the bed. In other words, per Eqs. (8), (11), and (15),

364 $\hat{\varepsilon}_l^B$ can be expressed approximately as follows:

$$365 \quad \hat{\varepsilon}_l^B = u_{w*}^2 \frac{dU'}{dy'} = \frac{u_{w*}^3}{\kappa s} \quad (32a)$$

366 where dU'/dy' is the depth-averaged velocity gradient in normal coordinates near the solid

367 wall. Based on the specifications of \hat{v}_l and Eq. (4), $(\hat{v}_l)_l^B$ can be expressed as $(\hat{v}_l)_l^B = \kappa s u_{w*}$;

368 \hat{k}_l^B can be written as follows:

369
$$\hat{k}_l^B = \frac{u_{w*}^2}{\sqrt{C_\mu}} \quad (32b)$$

370 u_{w*} must satisfy the following equation [24]:

371
$$\frac{U'}{u_{w*}} = \begin{cases} \frac{1}{\kappa} \ln \left(\frac{Eu_{w*}y'}{v_k} \right) & \text{for hydraulically smooth wall} \\ \frac{1}{\kappa} \ln \left(\frac{30y'}{k_s} \right) & \text{for hydraulically rough wall} \end{cases} \quad (33)$$

372 where $E = 0.9$ is the constant; U' is treated as a depth-averaged shear velocity at l ; both s
373 and y' are approximated by half of the normal space step at l .

374

375 To secure stable numerical results, the Courant-Friedrichs-Lewy (CFL) number Cr was
376 considered as the stability criterion within the proposed model and to enable its incorporation,
377 the following double stability conditions were imposed for Cr as suggested by the literature
378 [24]:

379
$$Cr_{\text{flow}} = \Delta t \max \left\{ \max \left[\left(\frac{|P|/H + \sqrt{gH}}{\Delta x} \right)_{i,j} \right], \max \left[\left(\frac{|Q|/H + \sqrt{gH}}{\Delta y} \right)_{i,j} \right] \right\} \leq 1 \quad (34a)$$

380
$$Cr_{\text{turbulence}} = \Delta t \max \left\{ \max \left[\left(\frac{2(\hat{v}_t + v_k)}{(\Delta x)^2} \right)_{i,j} \right], \max \left[\left(\frac{2(\hat{v}_t + v_k)}{(\Delta y)^2} \right)_{i,j} \right] \right\} \leq 1 \quad (34b)$$

381 where Δt is set as the minimum of the Δt values calculated by using Eqs. (34a) and (34b).

382 **3 Model Validations**

383 To validate the model previously described to quantify complex turbulence, its performance
384 has been verified against experimental turbulent flows obtained under various circumstances:

385 1) a uniform gravel bed, 2) a 90° bend, and 3) a suddenly expanding section. Numerical results
386 were then compared against measured datasets as well as the calculated values from the
387 standard $\hat{k} - \hat{\varepsilon}$ model and other numerical schemes. To distinguish among the different
388 models' results, "PF" and "RRF" are used to represent the model constructed by the proposed
389 formula and by Rastogi and Rodi's formula, respectively.

390 **3.1 Turbulent flow in a straight channel with gravel bed**

391 To verify the accuracy of the proposed model in replicating bed roughness and Reynolds
392 number effects on the formation of turbulent features, a series of experiments on open-channel
393 flows over rough beds conducted by Wang et al [38], were used for comparison. The

394 experiments were conducted in a straight flat glass flume 13.5 m long, 0.60 m wide, and 0.60
 395 deep [38]. The roughness elements on the bottom of the flume were composed of gravel with
 396 median diameter d_{50} ranging from 2 to 40 mm. Throughout all measurements, the simultaneous
 397 high-frequency velocities in the middle of the flume were obtained with an acoustic Doppler
 398 velocimeter (ADV).

399

400 According to the ensemble averages terms used in this study, velocity samples were gathered
 401 to determine the mean flows and turbulent fields in the system. The mean velocities in x -, y -,
 402 and z -directions were estimated as follows [24]:

$$403 \quad \bar{u} = \frac{1}{N} \sum_{i=1}^N u_i, \bar{v} = \frac{1}{N} \sum_{i=1}^N v_i, \bar{w} = \frac{1}{N} \sum_{i=1}^N w_i \quad (35)$$

404 where N is the number of samples. The root-mean-square (marked as r.m.s) values of the
 405 velocity fluctuations are defined by the sample standard deviation:

$$406 \quad \text{r.m.s. } u' = \sqrt{\frac{\sum_{i=1}^N u_i^2 - N\bar{u}^2}{N-1}}, \text{ r.m.s. } v' = \sqrt{\frac{\sum_{i=1}^N v_i^2 - N\bar{v}^2}{N-1}}, \text{ r.m.s. } w' = \sqrt{\frac{\sum_{i=1}^N w_i^2 - N\bar{w}^2}{N-1}} \quad (36)$$

407 The turbulent kinetic energy k can be calculated from the above definitions as follows:

$$408 \quad k = \frac{1}{2} \left[(\text{r.m.s. } u')^2 + (\text{r.m.s. } v')^2 + (\text{r.m.s. } w')^2 \right] \quad (37)$$

409

410 The corresponding depth-averaged \hat{k} can be obtained by depth-averaging the vertical profiles.
 411 The depth-averaged data calculated from vertical measured regions was taken to represent the
 412 entire depth at the corresponding horizontal coordinate due to the operation constraints of the
 413 ADV. The deviations between the depth-averaged velocities obtained by this method and those
 414 calculated by the logarithm profile in whole depth are around 5% [24].

415

416 The calculating dimensions in the numerical experiments were 4.0 m \times 0.6 m \times 0.6 m, which
 417 are consistent with the turbulent regime used by Wang et al. [38]. The roughness heights of the
 418 glass wall and the gravel bed were set to $k_s = 0.02$ mm and $k_s = d_{50}$, respectively [39]. k_s is the
 419 same in the glass bed as the wall. A uniform grid size $\Delta x = \Delta y = 0.02$ m and time step of
 420 0.002 s were used in the computation. Eleven typical cases of different gravel d_{50} and Reynolds
 421 numbers (Table 1) were analyzed. Considering the weight balance between the boundary
 422 conditions and fully turbulent development in regards to the effects of the turbulent structure in

423 the numerical flume, the inflow unit volume flux and outflow water depth were set to H_0U_0 and
424 H_0 , respectively.

425

426 According to the measurement results, \hat{k} was strongly dependent on the flow conditions when
427 k_s was constant and it increased as Re increased. It is demanding to make any definite
428 conclusion regarding the effects of k_s on \hat{k} , however, because it is too difficult to keep Re or
429 Fr neatly constant in any experiment. The ADV operation limitations and geometrical
430 inhomogeneity over the gravel bed were likely to be responsible for this phenomenon.

431

432 The numerical results of the models derived from different expressions of P_{kV} and $P_{\epsilon V}$ are also
433 presented in Table 1. The PF values deviate slightly from the measured data, but there is
434 reasonable agreement between them for the given ranges of k_s and Re . The RRF results
435 contained larger error than PF considering the whole range of results. The average of the error
436 for all the test cases C1 to C11, for the PF and RRF models are, respectively, 49.67 and
437 108.45%. With low bed roughness, $k_s < 5$ mm, both sets of results deviate gradually from the
438 experimental values as k_s decreases. This behaviour can be attributed to the anisotropic
439 tendency under which turbulent energy is redistributed over a smooth bed more slowly than
440 over a rough one, which may be enhanced as roughness size decreases. Overall, the results
441 show that the proposed model can effectively simulate turbulent flows over most of the gravel
442 bed.

443 **3.2 Turbulence of open-channel flow in a 90° bend**

444 Furthermore, the performance of numerical models PF and RRF and other models presented
445 by Cea et al. [11] was compared against turbulent flows in open channel with a 90° bend based
446 on the experimental conditions described by Bonillo [40]. The experimental setup was identical
447 to that described by Cea et al. [11], as shown in Fig. 3. The flow domain was made of two
448 straight flat sections linked by a 90° bend. The length and width of the first section were 4.835
449 m and 0.86 m, respectively; those of the second section were 4.43 m and 0.72 m, respectively.
450 The bed of Segment 1 is 0.013 m higher than the bottom of Segment 2. The bottom and two
451 sidewalls of the open channel are made of smooth concrete.

452

453 For calculation convenience and comparability among similar models, the flow region was
454 discretized using a uniform grid of $\Delta x = \Delta y = 0.02$ m. The Manning's coefficient of the bed
455 surface selected was the same as Cea et al.'s [11] 0.016 s/m^{1/3}. The roughness height of the

456 sidewall surface was assumed to be $k_s = 0.001m$ [39]. The time step was fixed to $\Delta t = 0.005s$ to
457 maintain numerical stability. The resulting \hat{k} values at three different cross sections are shown
458 in Fig. 4. The values calculated by two classical turbulence models [11], the *KE* model and
459 *RSM* model, are also included. Cea et al. [11] also developed a finite volume model to solve 2D
460 SWEs, in which two famous turbulence models were used for comparison. The *KE* model is
461 based on the assumption of isotropic eddy viscosity to solve the Reynolds stresses, while the
462 *RSM* model directly solves each Reynolds stress without any restrictive hypothesis. Though
463 the *KE* model equations are very similar to those of the *RRF* model, the location of H in the
464 diffusion term and the value of σ_ϵ in the former differ from those of the latter.

465

466 As shown in Fig. 4, the PF results are very close to the experimental data in both the left sidewall
467 area ($0 \leq x \leq 4.955$) and right sidewall region ($5.195 \leq x \leq 5.555$), where B is the width of the
468 channel. There are varying degrees of deviation in the numerical curves of the other three
469 models. In short, the flow features in both regions can be captured adequately by the PF model.
470 In the intermediate region ($4.955 \leq x \leq 5.195$), none of the numerical curves matched the
471 measured data. This may be because the basic assumption of the shallow water equations is
472 difficult to satisfy in the strong shear and bend zone, which includes intense 3D turbulence. The
473 proposed model yielded accurate results overall despite some data scattering in the shear region.

474 ***3.3 Turbulent characteristics in an expanding section***

475 An additional experiment was conducted to determine whether the proposed model can
476 simulate the turbulent flows on an expanding channel [24]. The experiment was carried out in
477 a flat expanding flume at the Hydraulic Engineering Laboratory at National University of
478 Singapore. The length, width, and depth of the flume are respectively 15 m, 0.6 m, and 0.6 m.
479 As shown in Fig. 5, the widths of the channel upstream and downstream of $x = 0$ are 0.3 m and
480 0.6 m, respectively. The steady flows were strictly controlled by two pumps and a tail gate
481 during the experiment; boundary conditions were the discharge at upstream ($0.024 \text{ m}^3/\text{s}$) and
482 the flow depth at downstream (0.015 m), respectively. 137 regular points of the intersection
483 were set between the longitudinal coordinates $x = -0.10, 0.25, 0.50, 0.75, 1.00, 1.25, 1.50, 1.75,$
484 $2.00, 2.25, 2.50, 2.75,$ and 3.00 m and the lateral coordinates $y = 0.05, 0.10, 0.15, 0.20, 0.25,$
485 $0.30, 0.35, 0.40, 0.45, 0.50,$ and 0.55 m to observe velocity profiles and further inspect
486 turbulence changes.

487

488 The three-dimensional flow velocities were measured with a SonTek/YSI 16-MHz MicroADV
489 with the sampling rate of 50Hz and the outputs of SNR and correlation factor from the

490 instrument were monitored following procedure already published in literature [24]. Similar to
491 the process in Section 3.1, the depth-averaged data (U , V , \hat{k} , and $\hat{\varepsilon}$) were further obtained.

492

493 We used identical numerical settings and discretization as Lin [24] to simulate turbulent flows
494 in this study. The computational analysis was performed in a rectangular region of
495 $9.0 \text{ m} \times 0.6 \text{ m}$ and differentiated by a 180×30 uniform grid with increments of $\Delta x = 0.05 \text{ m}$
496 and $\Delta y = 0.02 \text{ m}$; the length and width of the narrow channel upstream were 2.0 m and 0.3 m ,
497 respectively. The upstream and downstream boundary conditions were unit volume flux of
498 $0.08 \text{ m}^2/\text{s}$ and water depth of 0.15 m , respectively. The Manning coefficient of the bed was
499 $m = 0.01 \text{ s/m}^{1/3}$ and the sidewall was considered to be smooth. The time step used was
500 $\Delta t = 0.001 \text{ s}$.

501

502 The computed longitudinal velocities at different transverse sections were non-dimensionalized
503 by the approach velocity U_0 and compared against the experimental results as shown in Fig. 6.

504 In the upstream region without extension, i.e., $X_a = -0.1 \text{ m}$, the U -velocity distribution was highly
505 uniform. The sudden expansion in the profile of the sidewall induces strong non-uniformity to
506 the velocity profiles, which was clearly observable per the flow separation and wake region in
507 the detached flow. A recirculation zone (i.e., $0 \leq x/B \leq 8$), which was generated mainly due
508 to the stagnant effect of the right sidewall of the building and the southern boundary of the
509 channel, could also be clearly seen. In the downstream section, the longitudinal velocities
510 gradually tended towards uniformity. By contrast, the maximum forward and backward
511 velocities for both methods closely matched experimental data after the change in channel width,
512 especially in the circulation region.

513

514 Similar to the U -velocity profiles, the non-dimensional transversal velocities calculated by the
515 two models are shown in Fig. 7. In the main flow region (the area between $y = 0.3$ and 0.6 m),
516 the computed results agree fairly well with experimental data. A steep velocity gradient
517 occurred downstream of the building due to the strongly deflected flow. In the circulation zone
518 (from $y = 0.0$ to 0.3 m), the velocity changes computed via *RRF* method do not agree very well
519 with the experimental data. The proposed method agrees slightly better with the experimental
520 data but still underestimates the actual velocity by an average of about 50%. In that region, the
521 distribution of horizontal velocities is quite skewed over the full depth. The improved
522 turbulence model does not sufficiently offset the defect of the hydrodynamic assumption in the
523 deflected zone.

524

525 Figure 8 shows a comparison among computed \hat{k}/U_0^2 values and experimental data. The
526 proposed method yielded close agreement in the transverse section located $X_a=-0.1$ m upstream
527 of the abrupt extension, in which the statistical turbulence features are similar to the turbulent
528 characteristics in the open-channel uniform flow. The *RRF* results, by contrast, overestimated
529 by about 10%. At the upper-right corner of the building, where the flow separation began,
530 sizable boundary irregularities were a source of turbulent energy in the horizontal direction.
531 The horizontal bursts of turbulent activity propagated downstream and expanded on both sides,
532 forcing the \hat{k} values towards uniformity. Despite some scattering in the circulation zone, *PF*
533 yielded slightly more accurate results than *RRF* overall.

534

535 The dimensionless profiles of turbulent dissipation $\hat{\varepsilon}$ calculated by the two models were
536 compared against experiment data as shown in Fig. 9. In the main area and circulation zone,
537 the *PF* results were a better fit to the data than the *RRF* results. In the transitional region between
538 them, especially near the corner of the building, high levels of energy dissipation were produced
539 due to large-scale eddies and a steep velocity gradient. The proposed method better reflected
540 this phenomenon than the *RRF*, but still overestimated it by around 80%. The difference is
541 mainly attributable to experimental error due to ADV operation limitations and partly by the
542 strong 3D flow structure in corresponding regions. These results altogether indicate that *PF* can
543 better describe the hydraulic and turbulent structure in the abrupt expanding channel than *RRF*.

544 **4 Turbulent Flows near Two Groins in a Natural Waterway**

545 To further investigate the performance of the model developed and illustrate its engineering
546 application, it was used to compute complex turbulent flows and the correspondent navigation
547 conditions in natural waterways and waterways after the construction of two buildings.

548 ***4.1 Site description and numerical setup***

549 The Yangliu moraine is located in a relatively straight gorge on the upper reach of the Yangtze
550 River, approximately 1017.8 km upstream of Yichang City, a prefecture-level city in Hubei
551 Province, China. The length and width of the moraine are respectively 1800 m and 400 m, as
552 shown in Fig. 10. The top level of the moraine near the mid-channel, where the highest point is
553 5 m above the designed water level, is higher than the shoreline. To this effect, the unique bed
554 structure forms a concave basin. The water level in the river must be at least 1 m higher than
555 the designed level to satisfy the necessary flow conditions. Under the restriction of the moraine,
556 the main channel was squeezed to only 250 m in width. Another upstream moraine section of
557 the main reach, the Huangjia moraine, is affected by a shorter lateral flow area with 300 m. A

558 transitional shallow zone (width 500 m) was formed between the two moraines.

559

560 The transitional region, in which the flow is relatively slow, has a flat and straight geometric
561 bed. There is no erosion of river bed material along the ship route during the dry seasons due
562 to hydrodynamic limitations, hence there is only a small water depth for navigation during this
563 period. The minimum depths were recorded in 1993 and 2006, 2.3 m and 2.5 m, respectively.
564 Under these hydraulic conditions, it is very challenging to satisfy the class III navigation
565 conditions necessary for free travel of ships with dimensions 560 m × 50 m × 2.7 m .

566

567 To guarantee class III navigational standards throughout the entire year, the local waterway
568 bureau constructed two groins on the left side of the shallow region in 2008 (Fig. 10). Groin 1
569 was built at the upstream reach with a 60° angle between its axis and the main stream for
570 smooth flow transition. Groin 2 was constructed at the downstream end with a corresponding
571 angle of 75°. The length of the two groins are respectively 281 m and 313 m; both of their
572 hook heads are 87 m.

573

574 The local waterway bureau measured the bed topography of the reach, the water surface
575 elevation on the shipping route, and the flow velocity in three streamlines on January 15th, 2010,
576 to investigate the effects of the two groins on the waterway (Fig. 10) and the consequent
577 riverbed erosion. For this specific date, the total discharge recorded at the upstream section was
578 3120 m³/s and the average water level at the downstream section was 253.44 m, values derived
579 by a nearby hydrological station and a water gauge, respectively.

580

581 According to the geological analysis conducted to characterise the properties of the soil in the
582 two boreholes (N1 and N2, as shown in Fig. 10), the bed materials of the transitional shoal
583 region are mainly composed of boulders, sand-cobbles, and brick red sandstones. The mixture
584 of boulders and sand-cobbles typically forms a covering layer 2.3 m thick above the base layer
585 composed by sandstones. The maximum boulder particle-size is 0.9 m and the mass percentage
586 of sand-cobble with 0.03-0.2 m diameter is about 65%. The sieving results at N1 and N2
587 indicate that d_{50} in the reach is approximately 0.04 m.

588

589 The river section that was simulated within the model developed to verify its applicability is
590 1964 m long and 924 m wide, based on the topographic features of Yangliu and Huangjia
591 moraines (Fig. 10). The region that was computed was discretized by applying a uniform
592 Cartesian grid size with dimensions $\Delta x = \Delta y = 4$ m . The median particle size of the bed

593 material was set at $d_{50} = 0.04$ m and the time step was set at $\Delta t = 0.002$ s. A flow rate of 3120
594 m^3/s and an averaged water surface elevation of 253.44 m were respectively assigned to the
595 inflow and outflow boundaries according to the simplified methods presented by Zhang [41].

596 **4.2 Results and performance**

597 Figure 11 shows the comparisons between observed and simulated water levels along the ship
598 route. The average discrepancy between observed data and *PF* results is 0.124 m, while the
599 discrepancy between observed data and *RRF* results is 0.127 m. Although *PF* slightly
600 outperforms *RRF*, especially in the transition section, both have discrepancies from the
601 measured data. This is mainly due to the uniform roughness coefficient that was imposed in the
602 whole river, which does not replicate accurately the natural variety of roughness along the
603 system. In fact, the bed material is uneven in both longitudinal and transverse directions and
604 the bed structure is irregular in such a natural channel hence the bed resistance status could not
605 be characterised by a uniform median size as assumed in this study. Therefore, there is huge
606 potential to greatly improve the results if d_{50} was obtained at each specific site for the
607 numerical calculations.

608

609 The flow velocity along three different streamlines was computed and compared against the
610 measured values as shown in Fig. 12. Overall, the calculated curves agree well with the
611 experimental data except in the transition region of Streamline 2, where the maximum absolute
612 deviation was about 0.3 m/s. Similar to the measured water surface elevations, the surveyed
613 points of Streamline 2 were mainly distributed on the route. The d_{50} in the transitional area
614 was generally underestimated. Although there were no significant differences between the two
615 numerical results at most points, *PF* was more accurate than *RRF* near the two groins (the groins
616 are approximately at $x = 900$ and $x = 1200$ m, *PF* model is more accurate between $x \sim 800$ -1300
617 m). Because the turbulence parameters were not measured, we only depict the numerical \hat{k} at
618 two cross sections symbolically to reflect the relevant turbulence characteristics (Fig. 13). The
619 two sections, A-A and B-B (displayed as dash lines in Fig. 10 and their results presented in Fig.
620 13), are located downstream of the two groins where the longitudinal distance to the root of the
621 groin is approximately equal to the length of the corresponding groin (Fig. 10). As shown in
622 Fig. 13, the numerical values of *RRF* are about 2 times the *PF* results in the mainstream area
623 and approximately 1.5 times *PF*'s in the circulation zone behind the groin. Furthermore, for
624 each method, the numerical values at B-B were larger than those at A-A.

625

626 To further explore the navigation scenario discussed above, we calculated the water depth by
627 the proposed model as shown in Fig. 14. In the transitional region of a straight waterway, the

628 water depth was at least 3.5 m and the width of the water surface was greater than 80 m. To this
629 effect, the river would satisfy category III navigation conditions during the dry season. Our
630 results altogether showed that flow behavior in a natural river can indeed be captured with a
631 reasonable accuracy by the proposed method.

632 **5 Conclusions**

633 This study focused on developing a second-order numerical scheme of spatial staggered-grid
634 difference and temporal leap-frog discretization for simulating the turbulent flows on a complex
635 roughness bed. The model is based on the 2D SWE model and the $\hat{k} - \hat{\varepsilon}$ turbulent closure
636 model. The depth-averaged vertical turbulent generation from the universal notions of the
637 Kolmogorov -5/3 spectrum and the log-law was derived and used as a substitute for the vertical
638 velocity gradient term of the standard $\hat{k} - \hat{\varepsilon}$ model. The proposed $\hat{k} - \hat{\varepsilon}$ model reflects the
639 vertical turbulent production of various scales more robustly than the standard model.

640

641 Extensive comparisons were conducted against complex turbulent flows between the proposed
642 model, standard $\hat{k} - \hat{\varepsilon}$ model, and measurement data. The proposed method effectively
643 captured the experimental hydrodynamic features, especially the turbulence characteristics, and
644 improved the simulation accuracy over the standard $\hat{k} - \hat{\varepsilon}$ model. The proposed model also
645 showed better global performance than other 2D shallow numerical schemes.

646

647 Furthermore, the turbulent flows over the roughness bed in a natural river were simulated and
648 analyzed. Results showed that the depth-averaged turbulent energy increases as Reynolds
649 number increases when the roughness height is constant. Additionally, the numerical results for
650 Yangliu moraines reach showed that the river navigation conditions are satisfied after
651 constructing the two groins under the flow conditions we considered.

652

653 3D simulations will even more adequately disclose the fundamental physics of flows. In this
654 present model application, a large flow domain (Yangliu moraines reach) was considered hence
655 fully 3D computations would have not been very cost-effective. By using the proposed 2D
656 Shallow Water Equations with improved turbulence modelling techniques, it was possible to
657 achieve reasonably engineering accuracy but with a much lower CPU cost. Despite that,
658 considering that 3D analysis would provide a more accurate predictive tool for the flow
659 problems and promote a deeper understanding of the physics of the fluid motion, future work
660 will target the development of an enhanced quasi-three-dimensional shallow flow solver.

661

662 Per the large amplitude and gradient of turbulent energy near the structures, local scouring may
 663 occur in rainy seasons and gradually alter the bottom configuration, affecting the stability of
 664 the groins. To safeguard the regulation buildings, an effective sediment transportation model is
 665 necessary to investigate the bed deformation and future research should incorporate more cases
 666 to replicate accurately a variety of scenarios to achieve a universal model that can be reliable
 667 for each situation.

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 675 Discipline to Universities (Grant No: BC2018038).

676 **Notation**

677	f	= bed friction factor (-)
678	g	= gravitational acceleration (ms^{-2})
679	H	= water depth (m)
680	k	= turbulent energy (m^2s^{-2})
681	\hat{k}	= depth-averaged turbulent energy (m^2s^{-2})
682	k_s	= equivalent sand roughness (m)
683	l_m	= length scale of turbulent flow (m)
684	m	= Manning's roughness coefficient ($\text{sm}^{-1/3}$)
685	P, Q	= unit volume flux in x - and y -directions, respectively (m^2s^{-1})
686	R	= hydraulic radius (m)
687	Re	= Reynolds number (-)
688	T_{xx}, T_{yy}	= depth-averaged normal stress in x - and y -directions, respectively (Pa)
689	T_{yx}, T_{xy}	= depth-averaged shear stress in x - and y -directions, respectively (Pa)
690	u^*	= velocity scale of turbulent flow (ms^{-1})
691	u_*	= friction velocity (ms^{-1})
692	U, V, W	= depth-averaged velocity in x -, y - and z -directions, respectively (ms^{-1})

693	u, v, w	= instantaneous velocity in x -, y - and z -directions, respectively (ms^{-1})
694	$\bar{u}, \bar{v}, \bar{w}$	= ensemble-averaged velocity in x -, y - and z -directions, respectively (ms^{-1})
695	u', v', w'	= fluctuating velocity in x -, y - and z -directions, respectively (ms^{-1})
696	$\langle u \rangle, \langle v \rangle, \langle w \rangle$	= mean velocity in x -, y - and z -directions, respectively (ms^{-1})
697	$\ u'\ , \ v'\ , \ w'\ $	= turbulence intensity in x -, y - and z -directions, respectively (ms^{-1})
698	x, y, z	= streamwise, spanwise, and vertical coordinates, respectively (-)
699	z_b	= bed elevation (m)
700	ε	= turbulent dissipation (m^2s^{-3})
701	$\hat{\varepsilon}$	= depth-averaged turbulent dissipation (m^2s^{-3})
702	η	= free surface elevation (m)
703	ν	= turbulent viscosity (m^2s^{-1})
704	ν_k	= kinematic viscosity (m^2s^{-1})
705	$\hat{\nu}_t$	= depth-averaged turbulent viscosity (m^2s^{-1})
706	ρ	= fluid density (kgm^{-3})
707	τ	= total shear stress (Pa)
708	τ_b	= bed shear stress (Pa)
709		

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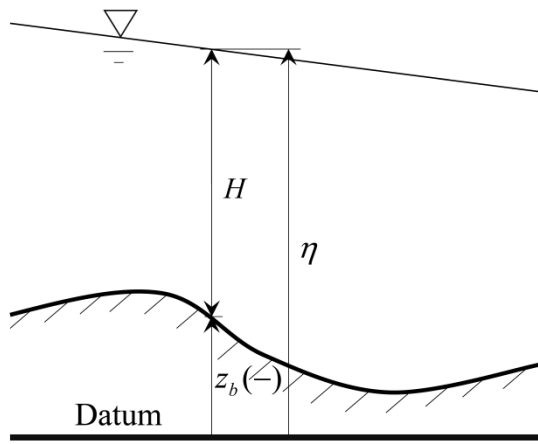
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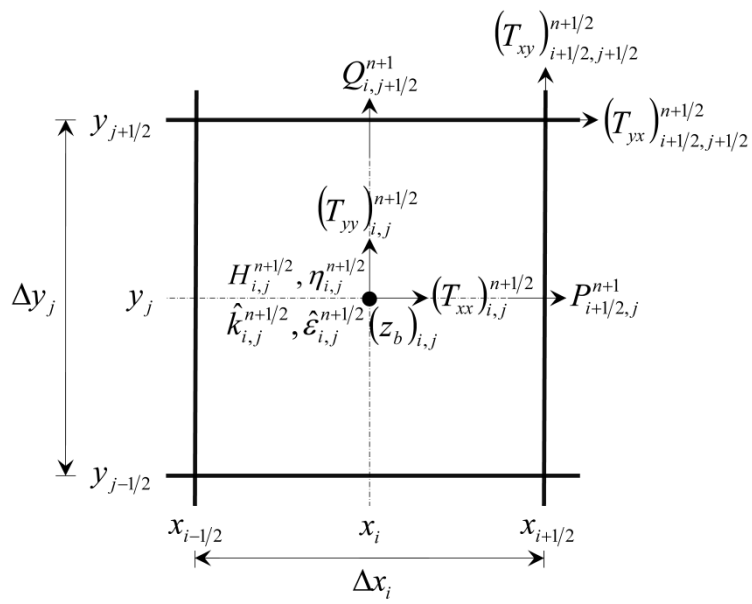


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807 Figure 1 - Scheme illustrating an example of irregular bed elevation and free surface water
808 depth.

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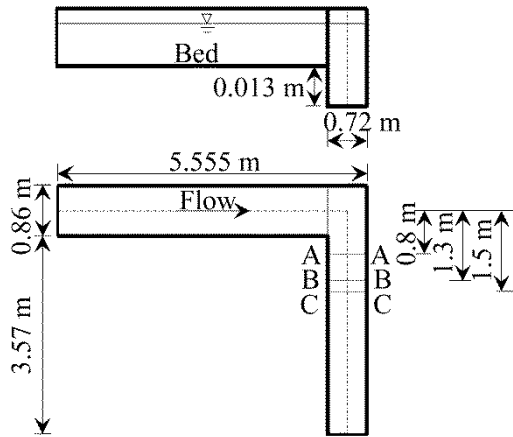


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812 Figure 2 - Scheme of staggered grid which includes the locations of the variables considered in
 813 a single cell.

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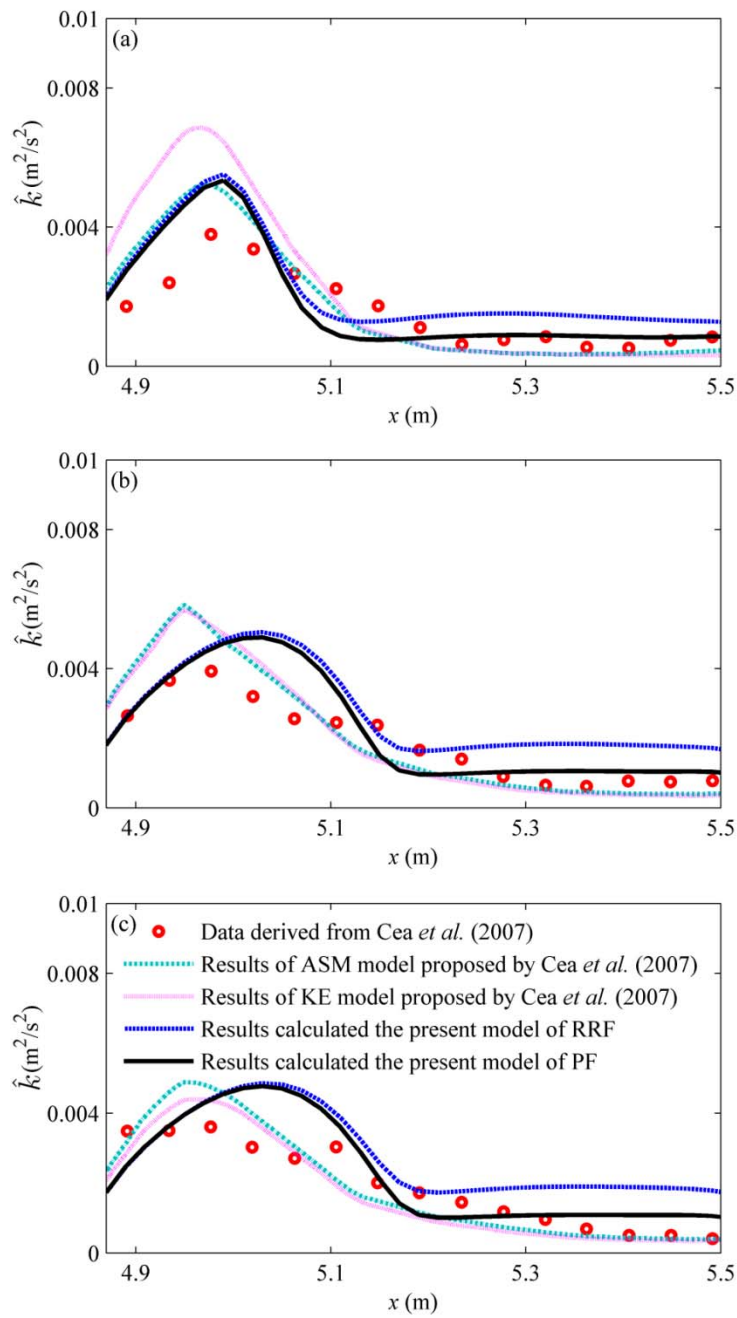


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817 Figure 3 – Scheme of the experimental channel with a 90° bend: front view (top) and top view

818 (bottom).

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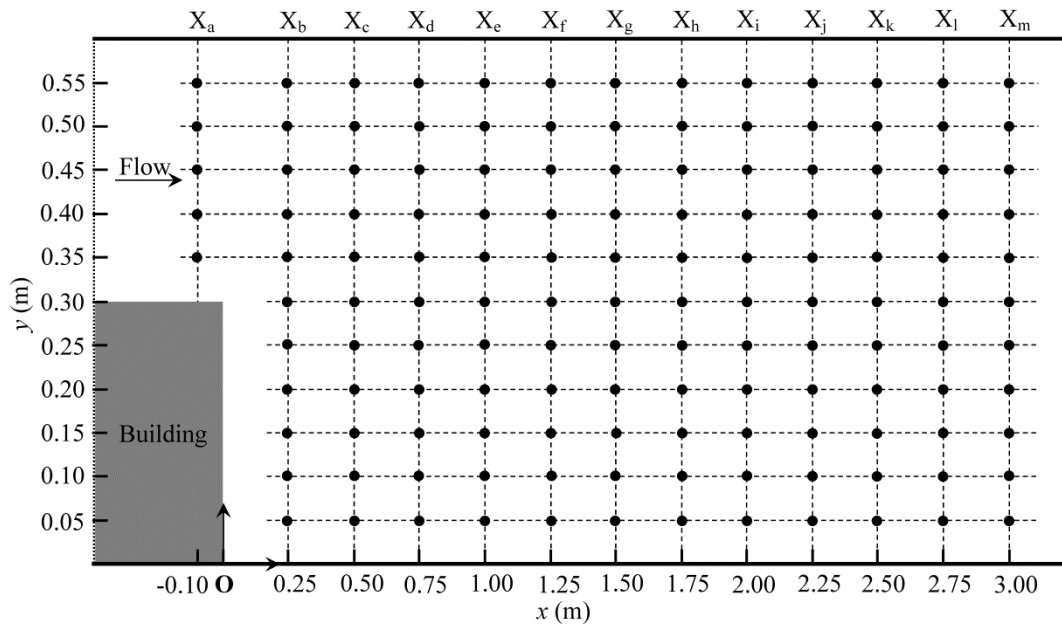
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822 Figure 4 – Comparison of turbulent kinetic energy measured experimentally and calculated

823 numerically at three sections (a) A-A, (b) B-B and (c) C-C.

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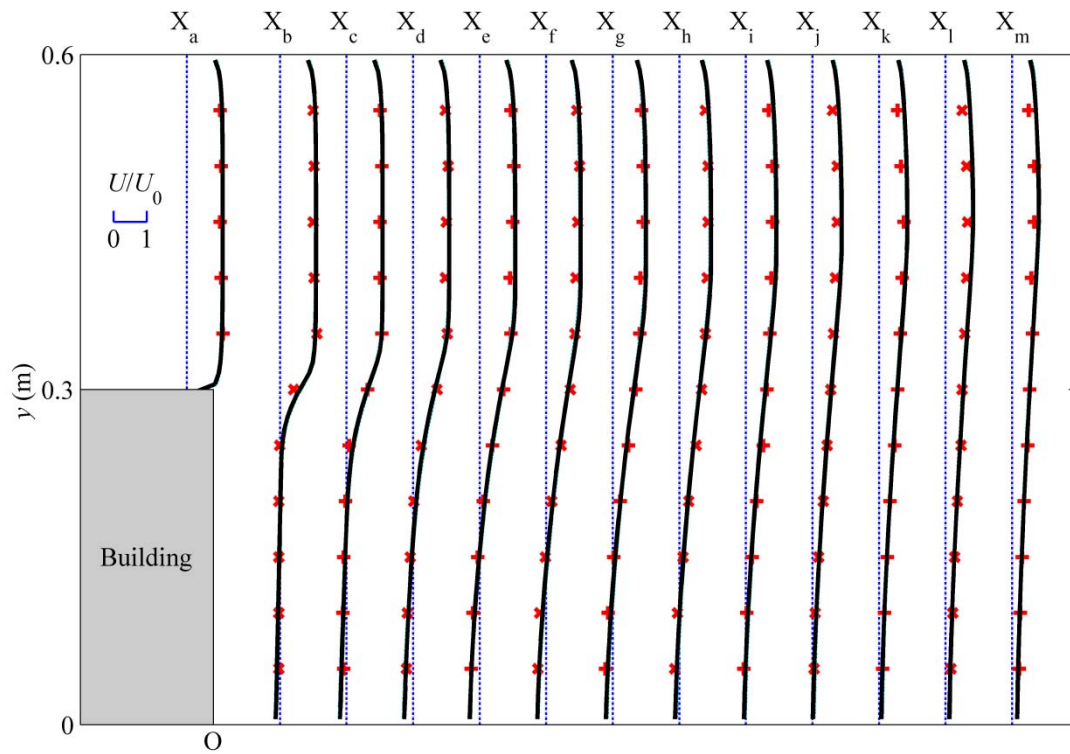
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827 Figure 5 - Plan view of flume with an expanding section and the observed points.

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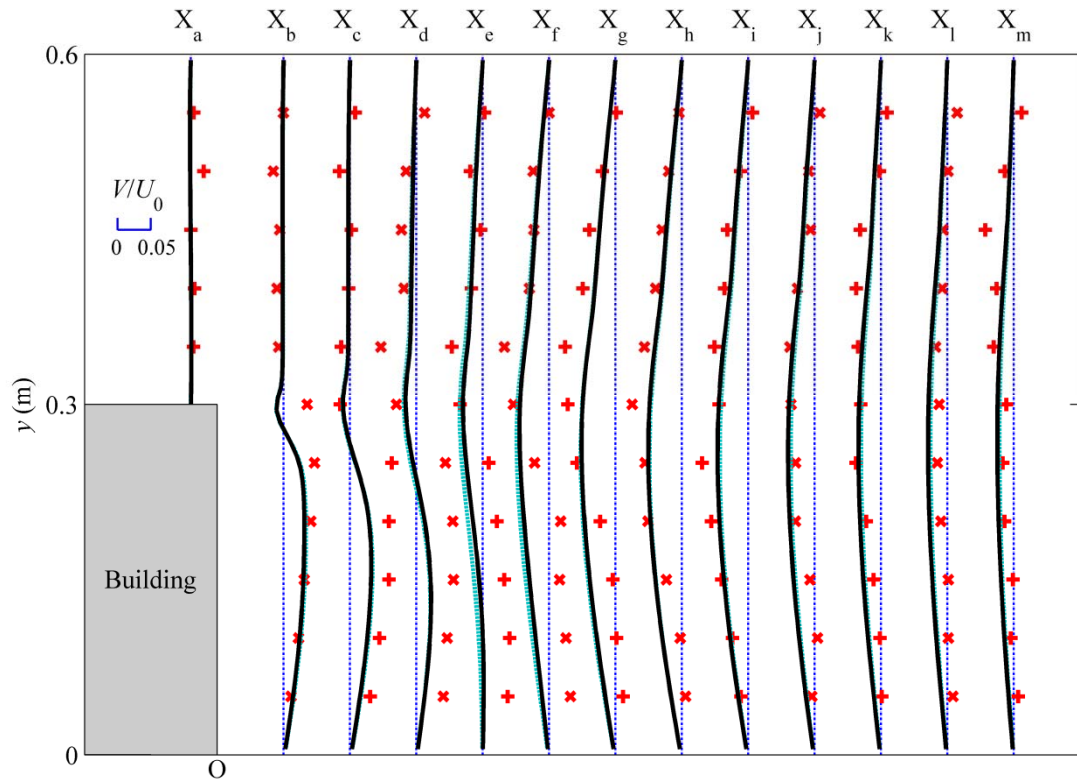


830

831 Figure 6 - Comparisons of non-dimensionalized U between numerical results and experimental
 832 data (Red crosses: experimental data; Dashed green line: RRF's results; Solid black line: PF's
 833 results).

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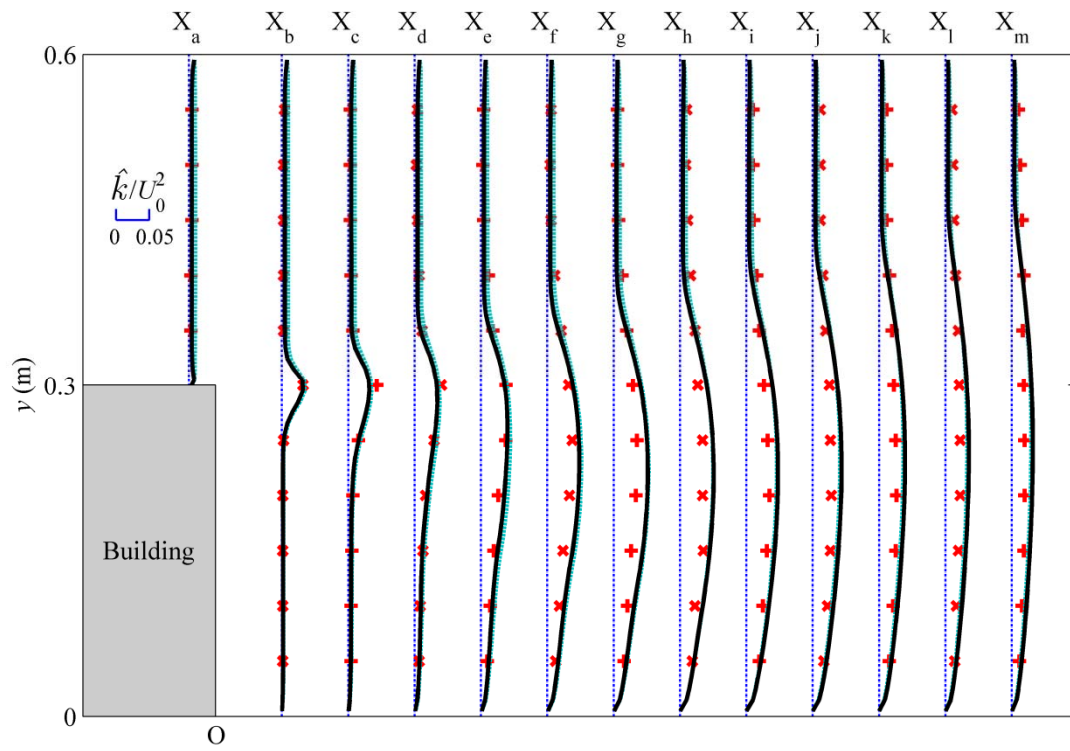


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837 Figure 7 - Comparisons of non-dimensionalized V between numerical results and experimental
838 data (Red crosses: experimental data; Dashed green line: RRF's results; Solid black line: PF's
839 results).

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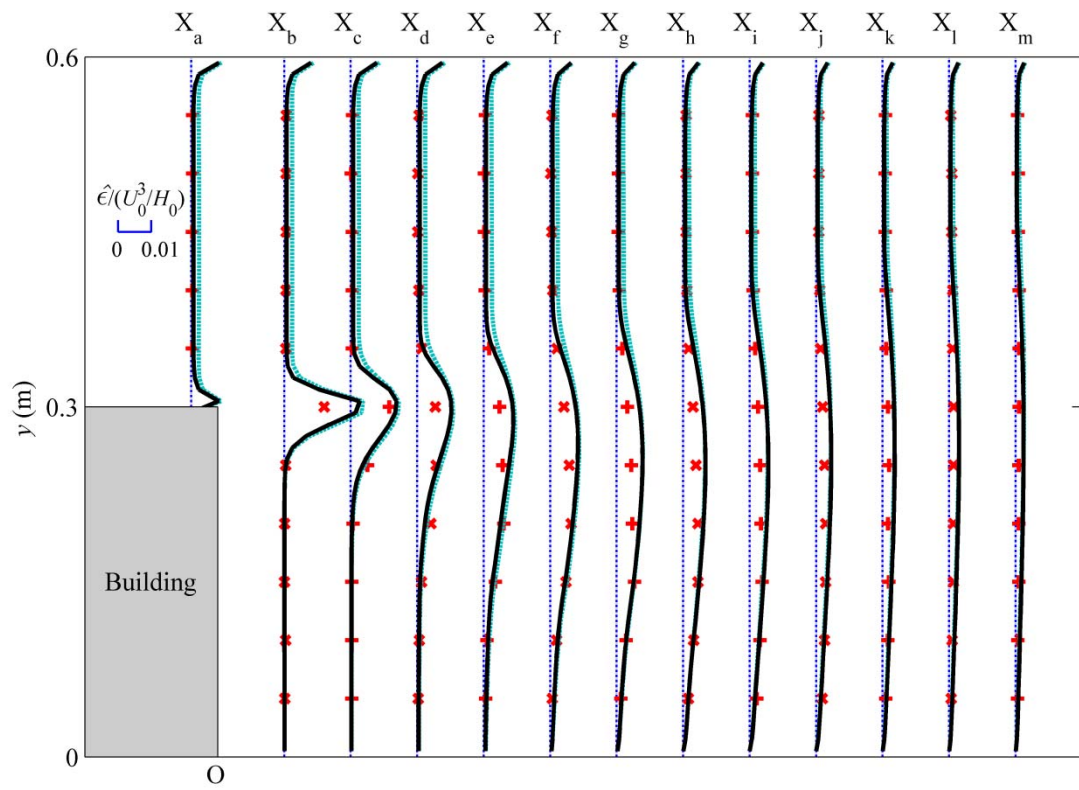


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843 Figure 8 - Comparisons of non-dimensionalized \hat{k} between numerical results and experimental
844 data (Red crosses: experimental data; Dashed green line: RRF's results; Solid black line: PF's
845 results).

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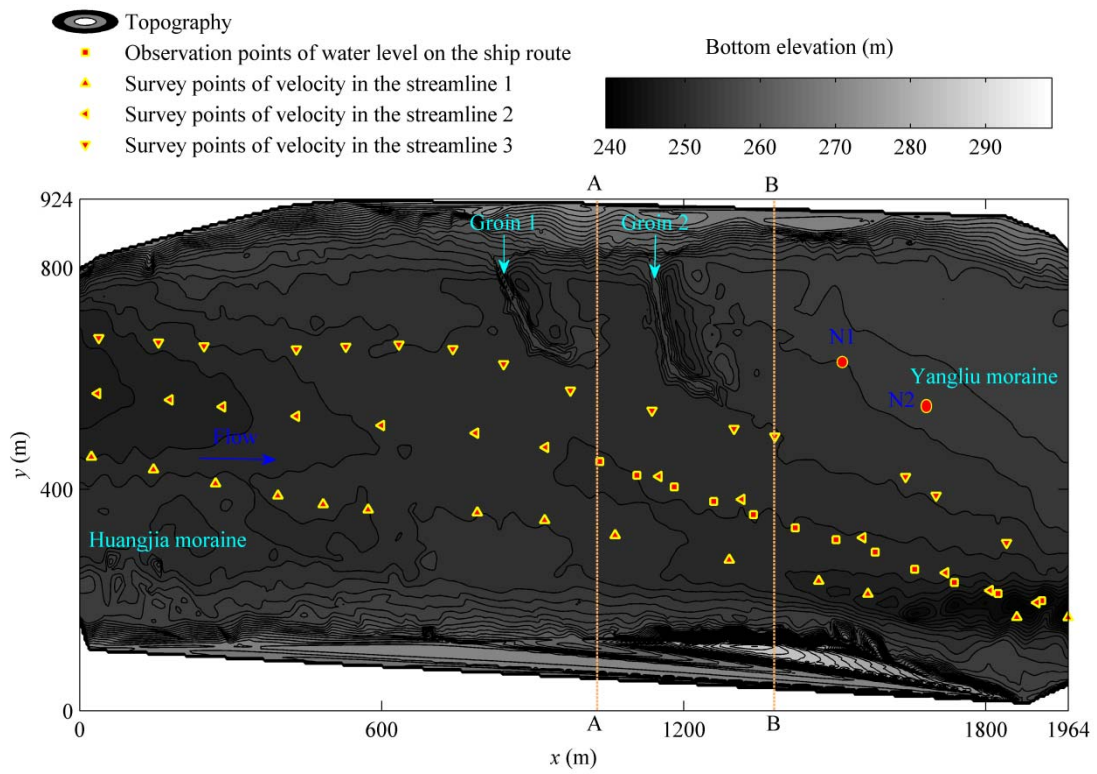


848

849 Figure 9 - Comparisons of non-dimensionalized $\hat{\epsilon}$ between numerical results and experimental
850 data (Red crosses: experimental data; Dashed green line: RRF's results; Solid black line: PF's
851 results).

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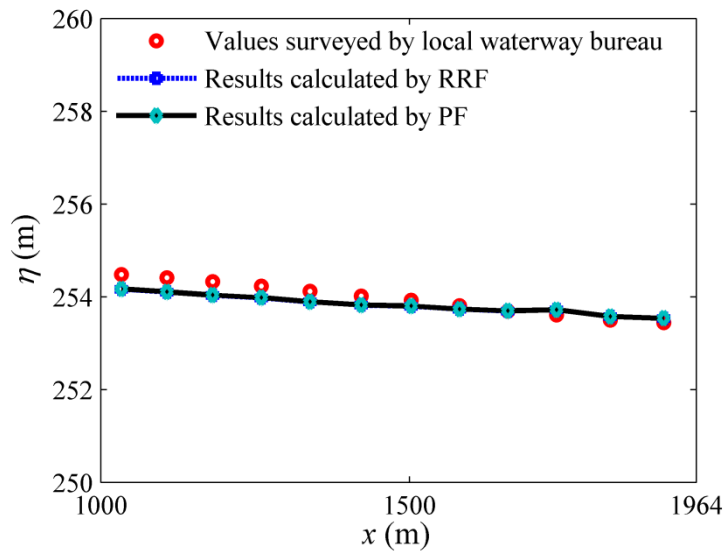


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855 Figure 10 - Bed topography of Yangliu moraine reach and location of observation points.

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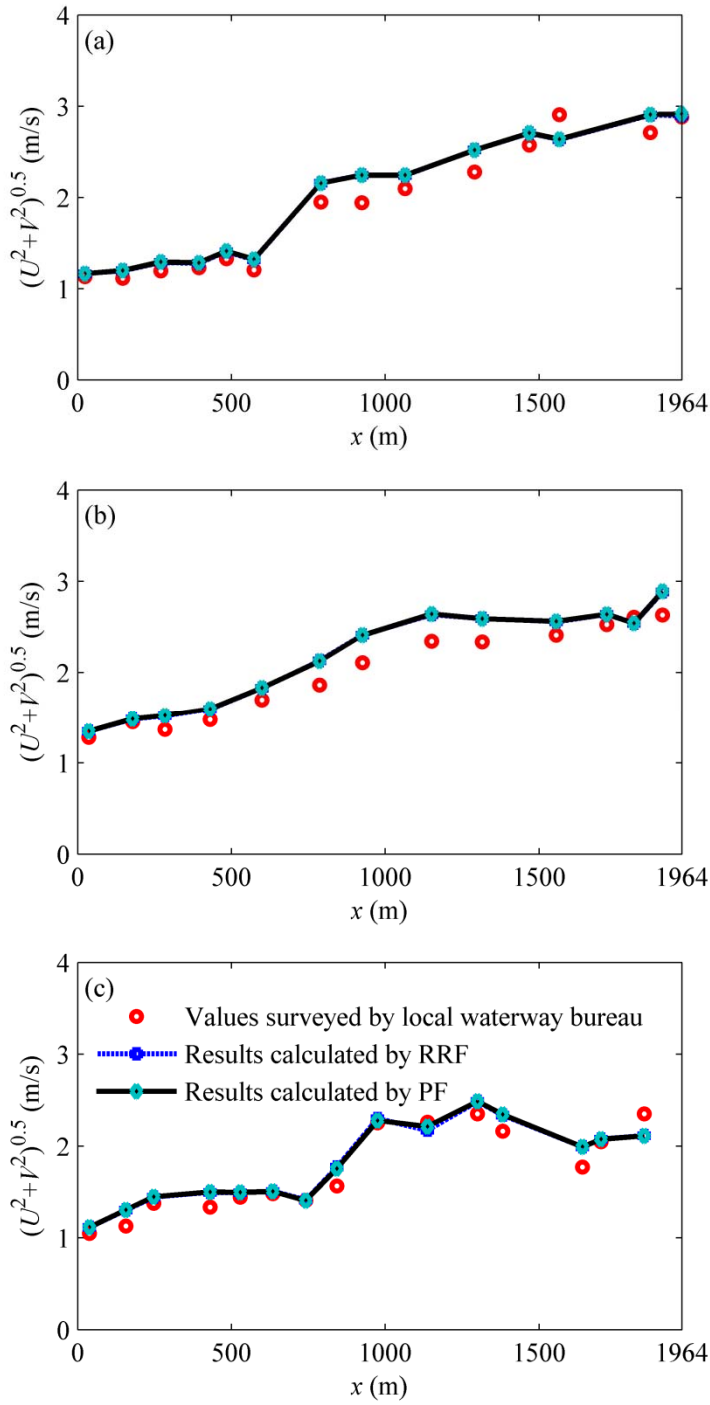
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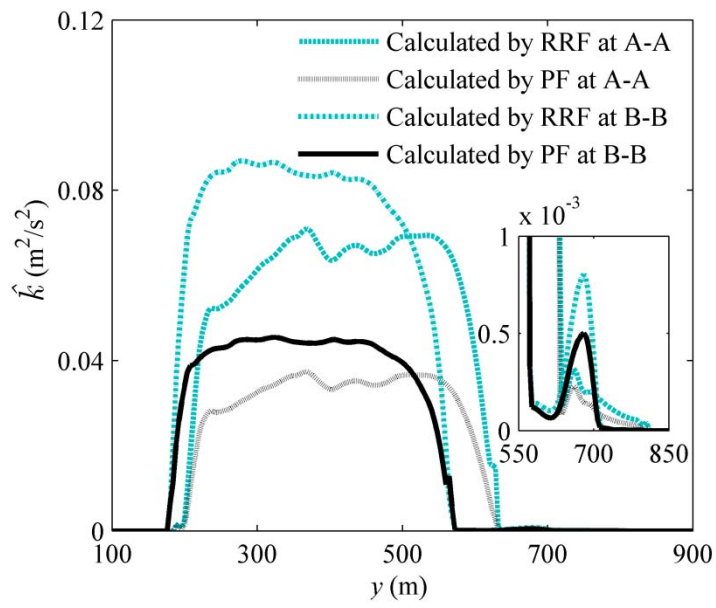
859 Figure 11 - Water level comparison between observed data and computed results on the ship
860 route.

861



864 Figure 12 - Flow velocity comparison between measured values and calculated results in the
 865 three streamlines: (a) streamline 1, (b) streamline 2 and (c) streamline 3.

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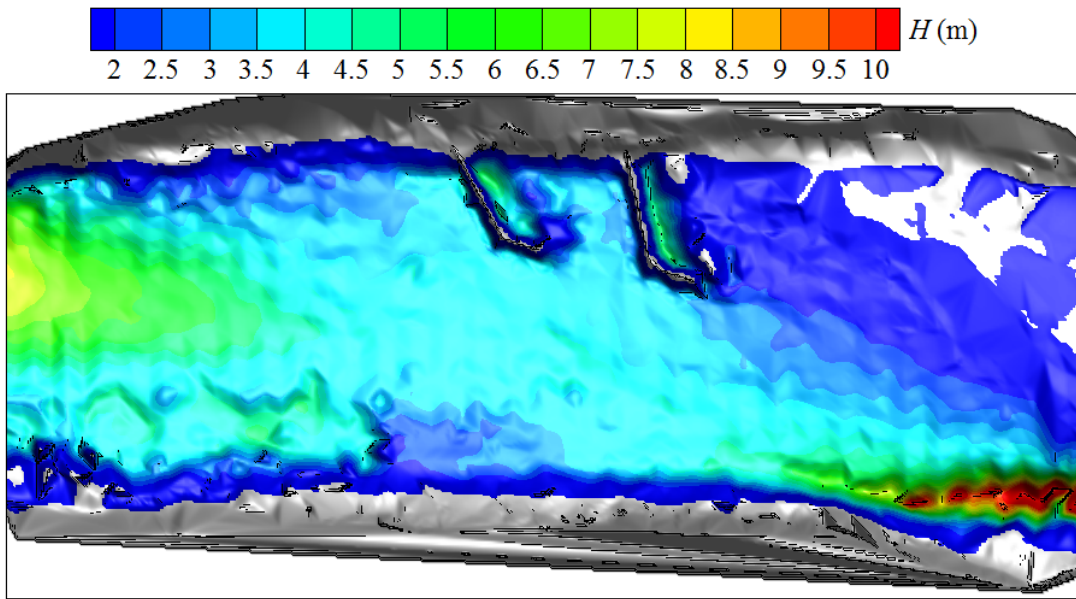


868

869 Figure 13 - Comparisons of the numerical results between PF and RRF at the sections of A-A
870 and B-B behind the two groins.

871

872



873

874 Figure 14 - Water depth calculated by the proposed model.

875

877 Table 1. Hydraulic data collected with the experiments and numerically calculated.

Case	k_s mm	H cm	U_0 cm/s	Re	Fr	\hat{k} acquired from measurements ($\times 10^{-3}$) m ² /s ²	\hat{k} simulated by PF		\hat{k} simulated by RRF	
							Results ($\times 10^{-3}$) m ² /s ²	Relative Absolute Error %	Results ($\times 10^{-3}$) m ² /s ²	Relative Absolute Error %
C1	0.02	50.2	34.0	170,680	0.15	2.83	0.33	88.3	0.77	72.8
C2	2	42.0	36.2	152,040	0.18	2.36	0.70	70.3	1.40	40.7
C3	5	24.8	65.3	161,944	0.42	3.41	3.20	6.2	5.83	71.0
C4	10	19.6	46.3	90,748	0.33	1.85	2.04	10.3	3.51	89.7
C5	10	30.7	57.8	177,446	0.33	3.81	2.84	25.5	5.02	31.8
C6	10	19.4	101.0	195,940	0.73	5.27	8.48	60.9	14.69	178.7
C7	20	31.8	42.7	135,786	0.24	2.35	1.84	21.7	3.12	32.8
C8	20	28.1	63.5	178,435	0.38	2.45	4.14	69.0	6.96	184.1
C9	40	28.8	35.4	101,952	0.21	0.89	1.55	74.2	2.49	179.8
C10	40	29.5	62.5	184,375	0.37	3.24	4.70	45.1	7.60	134.6
C11	40	17.5	110.5	193,375	0.84	7.22	12.63	74.9	20.00	177.0

878 k_s : gravel median diameter d_{50} , H and U_0 : average vertical distance from gravel bed to
879 water surface and bulk free-stream velocity in the middle section of the experimental flume,
880 respectively.

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